Sizing Tank Blanketing Regulators Using the Latest API 2000 7th Edition Guidelines

Author: Steve S. Attri, Global Product Manager, Emerson Process Management

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Introduction

In March of 2014, API Standard 2000 (Venting Atmospheric and Low-Pressure Storage Tanks) was revised. This Seventh Edition thus becomes the latest update. The subject of this article is how the latest changes affect the sizing of tank blanketing regulators, including backpressure ones used for vapor recovery systems.

Figure 1: The Latest Standard

The Fundamentals Remain Unchanged: Liquid Flow and Thermal Change

The first thing to understand is what has not changed. Namely, the fundamentals that impact tank pressure remain intact. This means that liquid flow (or pump-in and pump-out) and changes to temperature still form the fundamentals to the sizing calculations. Please see Figure 2.
Let’s take a closer look at the API Standard 2000 5th, 6th, and 7th Editions.

The API Standard 2000 5th Edition takes into account Tank Volume, Liquid Flow, and Temperature Change. It was written as a basis for the pressure control of hydrocarbons, and considered industrial tanks as well. It is this 5th Edition that is probably in widest use today.

In 2009, this was updated to the API Standard 2000 6th Edition. Note that the 5th Edition remained in the form of Appendix A, so it was not made obsolete per se. The additional factors of Average Storage Temperature, Vapor Pressure, and Latitude were added in the 6th Edition, as an additional focus was placed on alcohols which have higher vapor pressures and can significantly increase the inflow requirements.

This year, minor changes were implemented and the latest guideline is now the 7th Edition. One of the changes has to do with a simplified calculation for volatile liquids. Figure 3 summarizes the similarities and differences between the three latest editions of the standard.
Figure 3: A Comparison of Recent Standard Updates

New Variables: C-Factor & Y-Factor

Both the API Standard 2000 6th and 7th Editions include new variables in the calculations which depend on latitude. The key latitude categories are “Below 42 Degrees”, “Between 42 and 58 Degrees” and “Above 58 Degrees.” These latitude lines are where weather will patterns shift enough to cause meaningful differences in tank pressure.
As you can see in the Figure 5 tables, the C-Factor depends not only on latitude, but also on vapor pressure and average storage temperature. This C-Factor is used when making in-breathing flow calculations, which are required to size a tank blanketing regulator. The Y-Factor, on the other hand, is only dependent on latitude and is used when making out-breathing calculations, which are required to size a vapor recovery regulator.

<table>
<thead>
<tr>
<th>Latitude</th>
<th>C-Factor</th>
<th>Y-Factor</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Vapor pressure similar to Hexane</td>
<td>Vapor pressure higher than Hexane or unknown</td>
</tr>
<tr>
<td></td>
<td>&lt; 77 F</td>
<td>&gt; 77 F</td>
</tr>
<tr>
<td>Below 42 Deg</td>
<td>4</td>
<td>6.5</td>
</tr>
<tr>
<td>Between 42 &amp; 58 Deg</td>
<td>3</td>
<td>5</td>
</tr>
<tr>
<td>Above 58 Degrees</td>
<td>2.5</td>
<td>4</td>
</tr>
</tbody>
</table>

Figure 5: C-Factor and Y-Factor

Sizing Calculation for a Tank Blanketing Regulator

Let’s now turn to the sizing calculations themselves, starting with In-Breathing, which will determine the flow requirement for a tank blanketing regulator. The general steps are:

1. determine the volumetric flow rate required to replace the liquid being pumped out;
2. determine the volumetric flow rate required due to temperature drop;
3. add the results of (1) and (2) together.

\[
\text{Tank blanketing regulator flow} = \text{maximum pump out rate} + \text{temperature drop} \\
= [8.02 \times \text{maximum pump out rate}] + [3.08 \times \text{C-Factor} \times (\text{Tank Volume})^{0.7} \times \text{insulation factor}]
\]
To illustrate how this calculation, let’s consider the following example:

<table>
<thead>
<tr>
<th>Latitude</th>
<th>C-Factor</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Vapor pressure similar to Hexane</td>
</tr>
<tr>
<td></td>
<td>Average Storage Temperature</td>
</tr>
<tr>
<td></td>
<td>&lt; 77 F</td>
</tr>
<tr>
<td>Below 42 Deg</td>
<td>4</td>
</tr>
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<td>3</td>
</tr>
<tr>
<td>Above 58 Degrees</td>
<td>2.5</td>
</tr>
</tbody>
</table>

Tank blanketing regulator flow = maximum pump out rate + temperature drop

= [8.02 x maximum pump out rate] + [3.08 x C-Factor x (Tank Volume)^0.7 x insulation factor]

= [8.02 x 100] + [3.08 x (6.5) x (50,000 x 5.618)^0.7 x 1]

= 131,254 SCFH

Note that the insulation factor is 1 because there is no insulation. Also, the 5.618 constant converts barrels to cubic feet so that as result in SCFH can be obtained.
Implications of the New Guideline: In-Breathing

The latest API Standard 2000 7th Edition (and 6th Edition for that matter) result in greater In-Breathing requirements, and they may be much greater depending on the C-Factor which takes into account vapor pressure, average storage pressure, and latitude.

This is illustrated in Figure 6 which shows in-breathing requirements vs. tank size. The curve at the bottom of the graph depicts results using API Standard 2000 5th Edition, also known as Appendix A. Note that this curve ends at 180,000 barrels. This is because the scope of this edition was limited to this tank size. All of the other curves depict the 7th Edition, under different C-Factors. It can be seen that the relationship between in-breathing and tank size is not a linear one. The reason is that for smaller tanks, the tank surface to volume ratio is greater - and for larger tanks, the surface to volume ratio is smaller. This is why the curves start out linear and then tend to flatten out.

Figure 6: API Standard 2000 5th vs. 6th/7th Editions – In-Breathing
**Sizing Calculation for a Vapor Recovery Regulator**

Let’s now turn to the sizing calculations for out-breathing, which will determine the flow requirement for a vapor recovery regulator. The general steps in this case are:

1. determine the volumetric flow rate required to compensate for the liquid being pumped in;
2. determine the volumetric flow rate required due to temperature rise;
3. add the results of (1) and (2) together.

In the case of the out-breathing calculations, there are 2 sets of equations, one for non-volatile, and another for volatile liquids.

**Non-volatile liquids**

\[
\text{Vapor recovery regulator flow} = \text{maximum pump in rate} + \text{temperature rise} \\
= [8.02 \times \text{maximum pump in rate}] + [1.51 \times Y-\text{Factor} \times (\text{Tank Volume} \times 5.618)^{0.9} \times \text{Insulation Factor}]
\]

(Note that the constants 8.02 and 1.51 are to convert the result from metric to English units.)

**Volatile liquids**

\[
\text{Vapor recovery regulator flow} = \text{maximum pump in rate} + \text{temperature rise} \\
= [16.04 \times \text{maximum pump in rate}] + [1.51 \times Y-\text{Factor} \times (\text{Tank Volume} \times 5.618)^{0.9} \times \text{Insulation Factor}]
\]

Notice that the only difference between the equations for non-volatile and volatile liquids is that the 8.02 constant changes to 16.04 for volatile liquids. This is a key simplification mentioned earlier, that has been implemented with the 7th Edition of API Standard 2000. Volatile liquids will result in twice the out-breathing flow requirements as non-volatile ones.
To illustrate how this calculation works, let’s consider the same example once again:

Latitude → Below 42 Degrees
Vapor Pressure → Unknown
Average Storage Temp → 80 Degrees F
Tank Volume → 50,000 Barrels
Insulation → None
Max Pump In/Out → 100 Gallons/Min
Liquid Type → Volatile

<table>
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<tr>
<th>Latitude</th>
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<tbody>
<tr>
<td>Below 42 Deg</td>
<td>0.32</td>
</tr>
<tr>
<td>Between 42 &amp; 58 Deg</td>
<td>0.25</td>
</tr>
<tr>
<td>Above 58 Deg</td>
<td>0.20</td>
</tr>
</tbody>
</table>

Vapor recovery regulator flow = maximum pump in rate + temperature rise

= [16.04 x maximum pump in rate] + [1.51 x Y-Factor x (Tank Volume x 5.618)^0.9 x Insulation Factor]

= [16.04 x 100] + [1.51 x 0.32 x (50,000 x 5.618)^0.9 x 1]

= 40,314 SCFH
Implications of the New Guideline: Out-Breathing

Figure 7 shows a comparison of out-breathing requirements vs. tank size. The two curves indicated as Appendix A represent the API Standard 2000 5th Edition. There are two curves shown to illustrate both non-volatile and volatile liquids. The remaining curves depict results obtained using the 7th Edition, under different Y-Factor figures. The use of the latest guideline can result in greater out-breathing requirements, but not always. And, in general, when increased flow requirements result, they do not represent as much of a difference as do the in-breathing requirements explained earlier.
Conclusions

The latest API Standard 2000 7th Edition represents minor changes to the previous edition. However, it is important to recognize that the changes set forth by API Standard 2000 6th Edition remain intact. Although the 5th Edition continues to be widely used for sizing blanketing and vapor recovery regulators, it is expected that the newer editions will gain more acceptance and use in the years ahead.

These newer editions often result in greater flow requirements, especially for in-breathing. So it is important to recognize that the selection of the appropriate regulator may be impacted. Once the required flow is determined, other factors to consider would be the type of application, pipe size requirements, pressure, the desired set point, and the chemical compatibility of materials.